

Clausius - Clapeyron equation:

When two phases are in equilibrium, their chemical potential must be ~~in~~ equal.

$$\text{i.e. } \mu_\alpha(p, T) = \mu_\beta(p, T) \rightarrow \text{①}$$

where α and β are two phases in eq^{uu}.

By solving this eqⁿ ① for pressure in terms of temp, we can get an eqⁿ for the phase boundaries.

Let, P and T be changed infinitesimally so that two phases α and β remains in eq^{uu}. So, the change in chemical potential in the two phases must be equal.

$$\therefore d\mu_\alpha = d\mu_\beta \rightarrow \text{②}$$

$$\Rightarrow V_{\alpha,m} \cdot dp - S_{\alpha,m} \cdot dT = V_{\beta,m} \cdot dp - S_{\beta,m} \cdot dT.$$

where, $V_{\alpha,m}$ and $V_{\beta,m}$ are molar vol^m

of α & β .

$S_{\alpha,m}$ and $S_{\beta,m}$ are molar entropies

of α & β .

$$\left\{ \begin{array}{l} \therefore dG = Vdp - SdT \\ \Delta S = \frac{q}{T} \\ q \text{ is heat exchanged.} \end{array} \right.$$

$$\therefore (V_{\beta,m} - V_{\alpha,m}) \cdot dp = (S_{\beta,m} - S_{\alpha,m}) \cdot dT.$$

$$\Rightarrow \boxed{\frac{dp}{dT} = \frac{\Delta S}{\Delta V}}$$

$$\Rightarrow \boxed{\frac{dp}{dT} = \frac{q}{T \cdot \Delta V}} \quad \text{③}$$

This is Clapeyron eqⁿ and is application applicable to any phase eq^{uu} of any pure substance
for liquid \rightleftharpoons vapour, $q = \Delta_{\text{vap}} H$.

$$\therefore \text{eq ③} \Rightarrow \boxed{\frac{dp}{dT} = \frac{\Delta_{\text{vap}} H}{T \cdot \Delta V}}$$

Solid-Liquid Boundary:

Melting (fusion) is accompanied by molar enthalpy series, at fusion $\Delta_{\text{fus}} H$ and occurs at a temp T .
The molar entropy of melting is thus $\frac{\Delta_{\text{fus}} H}{T}$.

$$\frac{dP}{dT} = \frac{\Delta_{\text{fus}} H}{T \cdot \Delta_{\text{fus}} V}$$

Liquid-Vapour Boundary:

$$\frac{dP}{dT} = \frac{\Delta_{\text{vap}} H}{T \cdot \Delta_{\text{vap}} V} \rightarrow 0$$

Molar volm of a gas is so much greater than that of liquid we can write, $\Delta_{\text{vap}} V \approx V_m(g)$.

For perfect gas,

$$\Delta_{\text{vap}} V \approx V_m(g) = \frac{RT}{P}$$

$$\text{Eqn } 0 \Rightarrow \frac{dP}{dT} = \frac{\Delta_{\text{vap}} H}{T} \times \frac{P}{RT}$$

$$\Rightarrow \frac{1}{P} \cdot \frac{dP}{dT} = \frac{\Delta_{\text{vap}} H}{RT^2}$$

$$\Rightarrow \boxed{\frac{d(P)}{dT} = -\frac{\Delta_{\text{vap}} H}{RT^2}}$$

This is called

Clairius eqⁿ.

Integrated form: Clairius-Clapeyron eqⁿ.

Assuming that $\Delta_{\text{vap}} H$ remains constant over a small range of temp^r, we have from eqⁿ (i),

$$\int d(\ln P) = - \frac{\Delta_{\text{vap}} H}{R} \int \frac{dT}{T^2} .$$

$$\Rightarrow \ln P = - \frac{\Delta_{\text{vap}} H}{R} \times \frac{1}{T} + I . \quad \left\{ \begin{array}{l} I \text{ is integration} \\ \text{constant} \end{array} \right.$$

(iii)

Integrating eqn (iii) between limits of pressure P_1 and P_2 , corresponding to T_1 and T_2 , we get,

$$\int_{P_1}^{P_2} d(\ln P) = - \frac{\Delta_{\text{vap}} H}{R} \int_{T_1}^{T_2} \frac{dT}{T^2} .$$

$$\Rightarrow \ln \frac{P_2}{P_1} = - \frac{\Delta_{\text{vap}} H}{R} \left[\frac{1}{T} \right]_{T_1}^{T_2} .$$

$$\Rightarrow \ln \frac{P_2}{P_1} = - \frac{\Delta_{\text{vap}} H}{R} \left[\frac{1}{T_2} - \frac{1}{T_1} \right] .$$

$$\Rightarrow \ln \frac{P_2}{P_1} = \frac{\Delta_{\text{vap}} H}{R} \left[\frac{1}{T_1} - \frac{1}{T_2} \right] .$$

$$\Rightarrow \boxed{\log \frac{P_2}{P_1} = \frac{\Delta_{\text{vap}} H}{2.303 R} \left[\frac{T_2 - T_1}{T_1 T_2} \right]}$$

This is the integrated form of Clapeyron eqn and is called Clausius-Clapeyron eqn.